

In the Claims:

Claims 1-41 (Cancelled)

42. (Currently Amended): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H₂O with employing a low-pyrophoricity water-gas shift reaction catalyst; wherein the low-pyrophoricity water-gas shift reaction catalyst consists essentially of comprises alumina support particles with a mesh size of 12 or greater and a BET surface area of at least 10 m²/g impregnated with:
- (i) 0.5 to 25% by weight of an oxide of Ce, calculated as CeO₂, impregnated in the support particles, and
- (ii) between 4 and 14% by weight catalytic agent wherein the catalytic agent is Cu or an oxide thereof, calculated as CuO.
43. (Currently Amended): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H₂O with employing a low-pyrophoricity water-gas shift reaction catalyst; wherein the low-pyrophoricity water-gas shift reaction catalyst consists essentially of comprises alumina support particles with a mesh size of 12 or greater and a BET surface area of at least 10 m²/g impregnated with:
- (i) 0.5 to 25% by weight of an oxide of cerium, calculated as CeO₂ impregnated in the support particles;
- (ii) 0.5 to 10% by weight of an oxide of chromium, calculated as Cr₂O₃, impregnated in the support particles; wherein the combined concentration of the oxides of cerium and chromium is between 0.5 to 35% by weight; and
- (iii) between 4 and 14% by weight catalytic agent, wherein the catalytic agent is copper or an oxide thereof, calculated as CuO.

44. (Cancelled)

45. (New): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H₂O with a low-pyrophoricity water-gas shift

reaction catalyst; wherein the low-pyrophority water-gas shift reaction catalyst consists essentially of alumina support particles with a mesh size of 12 or greater and a BET surface area of at least 10 m²/g impregnated with:

- (i) 0.5 to 15% by weight of an oxide of chromium, calculated as Cr₂O₃, impregnated in the support particles, and
- (ii) between 4 and 14% by weight catalytic agent wherein the catalytic agent is Cu or an oxide thereof, calculated as CuO.

46. (New): The process of claim 42, wherein the input gas stream comprises:

- (i) between about 1% by volume and about 10% by volume CO,
 - (ii) at least 10% by volume hydrogen, and
 - (iii) at least 10% by volume H₂O; and
- wherein the input gas stream has a space velocity of at least 500 hr⁻¹ VHSV.
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47. (New): The process of claim 43, wherein the input gas stream comprises:

- (i) between about 1% by volume and about 10% by volume CO,
 - (ii) at least 10% by volume hydrogen, and
 - (iii) at least 10% by volume H₂O; and
- wherein the input gas stream has a space velocity of at least 500 hr⁻¹ VHSV.

48. (New): The process of claim 45, wherein the input gas stream comprises:

- (i) between about 1% by volume and about 10% by volume CO,
 - (ii) at least 10% by volume hydrogen, and
 - (iii) at least 10% by volume H₂O; and
- wherein the input gas stream has a space velocity of at least 500 hr⁻¹ VHSV.